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**EUROPEAN PATENT APPLICATION**

21 Application number: 90200611.3

51 Int. Cl.<sup>5</sup>: **B01J 21/06, B01J 37/00**

22 Date of filing: 14.03.90

30 Priority: 23.03.89 GB 8906726

43 Date of publication of application:  
26.09.90 Bulletin 90/39

84 Designated Contracting States:  
**AT BE CH DE DK ES FR GB GR IT LI LU NL SE**

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54 **Titania extrudates.**

57 The invention relates to a process for the preparation of a shapable dough which comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture, to a shapable dough obtained by this process, to the preparation of titania extrudates therefrom and to their use as catalyst carriers in hydrocarbon conversion processes, in hydrogenation processes, in hydrocarbon synthesis processes or in the purification of exhaust gases.

**EP 0 389 041 A1**

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## TITANIA EXTRUDATES

The present invention relates to the preparation of titania extrudates, to the preparation of a shapable dough for titania extrudates, to a shapable dough for titania extrudates and to the preparation of calcined titania extrudates and to their use.

Titania is a well-known material, which is often used as catalyst carrier or catalyst in various processes. It should be noted that the titania-containing catalyst systems described in the art are invariably based on titania powder, which does not make such systems directly suitable for industrial applications. In order to bring titania into an industrially more appropriate form it has been recently described in DE-C-3217751 to produce titania pellets by pelletising pyrogenically manufactured titania using a certain class of pelletising agents such as polyvalent alkanols and, in particular, graphite in powder form.

Thusfar, it has not been possible to extrude titania like other carriers such as alumina in conventional extrusion equipment to give reasonably strong products. Since titania is an interesting carrier material, especially in the absence of binder material, it was considered important to investigate whether this notoriously difficult to shape material could be subjected to an extrusion process to obtain titania extrudates of sufficient strength to be of industrial importance.

It has now been found that titania extrudates can be suitably prepared when use is made of an alkanolamine or ammonia or an ammonia-releasing compound in the preparation of a dough from which titania extrudates can be obtained.

The present invention therefore relates to a process for the preparation of a shapable dough which comprises mixing and kneading a particulate titania with water and with an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture.

The invention further relates to a process for the preparation of titania extrudates which comprises mixing and kneading a particulate titania with water and with an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture and extruding the mixture.

The invention further relates to a process for manufacturing calcined titania extrudates which comprises extruding a shapable dough into titania extrudates and drying and calcining the titania extrudates to a final temperature of between 300 °C and 1000 °C, and to calcined titania extrudates obtained by said process.

The titania to be used in the process according to the present invention can be both of rutile and of anatase nature. Also mixtures of both forms of titania can be suitably applied. In the event that it is necessary or advisable to use titania containing both rutile and anatase it will be clear that the preferred rutile:anatase ratio to be applied will be depending to some extent on the particular application concerned. Generally, ratios ranging between 0.66:1 and 100:1 can be suitably applied. When aiming at synthesis gas conversion reactions preference is given to the use of rutile:anatase ratios of at least 2:1. Examples of a suitable titania source comprise commercially available P25 (Degussa), a low surface area titania (a mixture of anatase and rutile) and a high surface area material consisting of anatase. Also various forms of pyrogenically produced titania can be used in the preparation of the shapable doughs and the corresponding extrudates in accordance with the present invention.

The total solids content of the mixture of titania, alkanolamine or ammonia or ammonium-releasing component (expressed as ammonia) and water ranges from 50 to 85% by weight, preferably from 55 to 80% by weight and more preferably from 60 to 75% by weight, in order to obtain an extrudable mixture.

The amount of alkanolamine or ammonia or ammonia-releasing component (expressed as ammonia) ranges from 0.5 to 20% by weight, preferably from 2 to 15% by weight, more preferably from 3 to 10% by weight, calculated on the total solids content.

Suitable, ammonia-releasing compounds other than  $\text{NH}_4\text{OH}$  or alkanolamines can be used in the formation of the shapable doughs and the extrudates produced therefrom. Ammonia-releasing compounds are defined for the purpose of the present invention as compounds capable of releasing  $\text{NH}_3$  gas on decomposition, e.g. under the influence of heat.

Suitable alkanolamines to be used in the process according to the present invention comprise the mono-, di- and tri- alkanolamines. Preferred are monoalkanolamines, such as those containing 2 to 10 carbon atoms, e.g. ethanolamine, propanolamine, hexanolamine, nonanolamine and decanolamine. Other examples of suitable alkanolamines comprise diethanolamine and triethanolamine. Preference is given to the use of monoethanolamine. If desired, mixtures of alkanolamines or mixtures comprising ammonia and

one or more alkanolamines can be suitably applied.

To improve the flux properties in the extruder the dough to be extruded may also comprise a polyelectrolyte, such as Nalco 7879 (obtainable from Nalco). The dough to which a polyelectrolyte may be added can readily be extruded e.g. over the metal die-plate of a Bonnot-extruder. Cylindrical extrudates can be prepared, but other forms may be prepared as well, such as mentioned, for instance, in US patent specification 4,028,227. The surface area of the titania extrudates ranges suitably between 40 and 300 m<sup>2</sup>/g depending on the starting titania used in preparing the shapable dough.

It has been found that the surface areas of the titania extrudates produced are dependent to some extent of the surface area of the starting powder material. When using powders with relatively low surface areas, the extrudates produced have typically similar surface areas, whereas the use of powders having relatively large surface areas may well lead to extrudates having considerable lower surface areas, e.g. some 30 to 50% lower, but still sufficiently larger than obtained when starting from a low surface area powder.

It is possible, though not necessarily advantageous, to add other oxides such as silicium dioxide and/or zirconium dioxide to the composition to be extruded. Amounts of up to 50%, but preferably of not more than 20% by weight of other oxides may be present in the composition to be extruded. It has been found that the presence of rather large amounts of other oxides may have a detrimental effect on the strength of the extrudates produced.

It is also possible to incorporate other materials such as crystalline (metallo)silicates, in particular zeolites, such as zeolite Y, into the dough to be extruded so as to arrive at zeolite-containing titania extrudates which have considerable strength.

After extrusion, the titania-containing extrudates are subjected to drying and normally also to calcining. Drying is suitably carried out by subjecting the extrudates to a mild heat treatment, e.g. at a temperature of up to 150 °C to remove water still present in the extrudates. Good results have been obtained using a drying temperature of about 120 °C.

The calcination of the extrudates is normally carried out at a temperature in the range between 300 °C and 1000 °C. Preferably, the calcination is carried out at a temperature in the range of from 450 °C to 750 °C, most preferably in the range of from 475 °C to 725 °C.

The titania extrudates can be suitably used, for example, as carriers for catalysts which are normally used in hydroconversion processes, like the hydrodemetallization and hydrodesulphurization of heavy hydrocarbon oils, in the hydrogenation of hydrogenatable components or hydrocarbon fractions such as kerosene and various types of cycle oils, in hydrocarbon synthesis reactions, in the epoxidation of olefinically unsaturated compounds with organic hydroperoxides, in the hydration of olefinically unsaturated compounds to produce the corresponding alkanols and in the purification of exhaust gases, in particular in the denoxing of nitrogen containing oxygenates.

Examples of hydrocarbon synthesis reactions comprise Fischer-Tropsch type reactions aimed at producing (long chain) hydrocarbons from carbon monoxide and hydrogen. In particular, the titania extrudates loaded with suitable Fischer-Tropsch metal(s), e.g. Group VIII metals as iron, nickel or cobalt, optionally containing one or more promoters such as zirconia or rhenium, can be suitably applied in the heavy paraffin synthesis step which is one of the process steps in an integrated process for the manufacture of middle distillates starting from methane to produce a syngas mixture which serves as starting material for the heavy paraffin synthesis and wherein the heavy paraffins produced are subjected to a catalytic heavy paraffin conversion process to produce the desired middle distillates.

The invention will now be illustrated by means of the following Examples.

#### EXAMPLE I

A mixture was prepared having the following composition

titania (ex Degussa)	74.5 g
water (demineralized)	32.5 g
monoethanolamine (MEA)	2.6 g
total	109.6 g

The mixture was prepared by adding the MEA and water to the titania and the mixture was kneaded for 30 minutes. The resulting mix was extruded on a laboratory extruder. The obtained extrudates (1.5 mm) were dried at 120 °C for 2 hours and calcined for 2 hours at 500 °C.

The titania obtained had the following properties:

BET surface area 52 m<sup>2</sup>/g  
medium pore diameter 32 nm  
pore volume 0.29 ml/g

#### EXAMPLE II

The experiment as described in Example I was repeated using a mixture containing 200 g of titania powder, 80 g of water and 8 g MEA. The mixture was kneaded for 45 minutes and then subjected to extrusion, drying and calcining as described in Example I. The titania obtained had the following properties:

BET surface area 51 m<sup>2</sup>/g  
medium pore diameter 39 nm  
pore volume 0.36 ml/g  
bulk crushing strength 0.59 MPa

#### EXAMPLE III

The experiment as described in Example I was repeated using 150 g titania powder, 30 g water and 30 g ammonia (25%). The mixture was kneaded for 20 minutes. Subsequently, two batches of 10 g water were added and the mixing was continued for another 25 minutes. The mixture was extruded, dried and calcined as described in Example I. The titania obtained had the following properties:

BET surface area 47 m<sup>2</sup>/g  
medium pore diameter 27 nm  
pore volume 0.30 ml/g  
bulk crushing strength 0.62 MPa

#### EXAMPLE IV

A mixture was prepared having the following composition

titania (ex TIL)		228 g
water		110 g
MEA		5 g
	total	343 g

The mixture was kneaded for 45 minutes. The mixture was then extruded, dried and calcined as described in Example I. The titania obtained had the following properties:

BET surface area 82 m<sup>2</sup>/g  
medium pore diameter 37 nm  
pore volume 0.36 ml/g  
bulk crushing strength 0.25 MPa

#### EXAMPLE V

A mixture was prepared from 114 g titania (ex TIL) and 107 g silica (ex Crossfield). To this mixture were added 5 g MEA and 150 g water. During the next 45 minutes, another 60 g of water was added in small portions. The resulting mix was extruded, dried and calcined at 700 °C for 2 hours. The titania-silica obtained had the following properties:

BET surface 192 m<sup>2</sup>/g  
 medium pore diameter 22 nm  
 pore volume 0.76 ml/g  
 bulk crushing strength 0.33 MPa

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#### EXAMPLE VI

A mixture was prepared from 150 g titania (ex Degussa), 7.5 g of MEA and 50 g of water. To this  
 10 mixture was added 111 g of a zeolite Y having a silica/alumina molar ratio of 40, and 50 g of water. After 15  
 minutes another 15 g of water was added. The resultant mixture was smoothly extruded. It was then dried  
 at 120 °C and calcined at 500 °C for 2 hours. The titania-zeolite Y obtained had the following properties:  
 BET surface area 246 m<sup>2</sup>/g  
 medium pore diameter 32 nm  
 15 pore volume 0.33 ml/g  
 bulk crushing strength 0.90 MPa

#### EXAMPLE VII

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1.6 mm Extrudates prepared in accordance with the experiment described in Example VI were  
 impregnated with a solution of H<sub>2</sub>PtCl<sub>6</sub> made up to allow after reduction with hydrogen at 400 °C a Pt-  
 content of 0.8% by weight on titania.

The catalyst thus prepared was used in a hydrogenation experiment. The hydrogenation experiment  
 25 was carried out using a hydrotreated light cycle oil containing 273 mmol monoaromatics/100 grammes. Its  
 90% by weight boiling point amounted to 351 °C and it contained 112 ppmw (parts per million by weight)  
 of sulphur and 7.6 ppmw of nitrogen. The experiment was carried out at a pressure of 50 bar and at a  
 temperature of up to 340 °C. It was found that the monoaromatics content had been reduced to about 70  
 mmol/100 grammes.

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#### Claims

1. A process for the preparation of a shapable dough which comprises mixing and kneading a  
 35 particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain  
 a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being  
 present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture.
2. A process according to claim 1 wherein the total solids content is from 50 to 80% by weight,  
 preferably 60 to 75% by weight.
3. A process according to claim 1 or 2 wherein use is made of anatase and/or rutile as titania source.
4. A process according to one or more of claims 1-3 wherein use is made of an alkanolamine or  
 ammonia in an amount between 2 and 15% by weight, preferably between 3 and 10% by weight.
5. A process according to one or more of claims 1-4 wherein use is made of a mono-, di- or  
 trialkanolamine having 2 to 10 carbon atoms.
- 45 6. A process according to claim 5 wherein use is made of monoethanolamine.
7. A process according to one or more of claims 1-6 wherein at most 50% by weight of silica and/or  
 zirconium dioxide and/or a zeolite, preferably a zeolite Y, is admixed.
8. Shapable dough whenever prepared by means of a process as claimed in one or more of claims 1-7.
9. A process for the preparation of titania extrudates from a shapable dough according to claim 1, which  
 50 comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an  
 ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight,  
 the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids  
 content of the mixture and extruding the mixture.
10. A process according to claim 9 which comprises mixing and kneading a particulate titania with water  
 55 and an alkanolamine having 2 to 10 carbon atoms or ammonia to obtain a mixture having a total solids  
 content of from 60 to 75% by weight, the alkanolamine or ammonium being present in an amount of from 3  
 to 10% by weight on the total solids content of the mixture and extruding the mixture.
11. Titania extrudates whenever prepared by means of a process according to claim 9 or 10.

12. A process for manufacturing calcined titania extrudates which comprises drying and calcining the titania extrudates according to one or more of claims 9-11 to a final temperature of between 300 °C and 1000 °C.

13. A process according to claim 12 wherein the calcination is carried out at a temperature in the range between 450 °C and 750 °C, preferably in the range between 475 °C and 725 °C.

14. Calcined titania extrudates whenever manufactured by means of a process according to claim 12 or 13.

15. Use of titania extrudates according to claim 14 as catalyst carriers in hydrocarbon conversion processes, in hydrogenation processes, in hydrocarbon synthesis reactions or in the purification of exhaust gases.

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# EUROPEAN SEARCH REPORT

Application Number

EP 90 20 0611

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
X	FR-A-2 231 423 (BRITISH STEEL) * Page 2, lines 3-24; claims 1,2; page 1, lines 11-36 *	1,3,8,9 ,12,14	B 01 J 21/06 B 01 J 37/00
Y	---	2,7	
Y,A	EP-A-0 038 741 (RHONE-POULENC) * Claims *	2,7	
A	DE-A-2 426 496 (BRITISH STEEL) -----		
			TECHNICAL FIELDS SEARCHED (Int. Cl.5)
			B 01 J
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 04-07-1990	Examiner THION M.A.
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